

# 90% Multi-Poise Condensing Furnaces Heat Exchanger and Sooting



Turn to the Experts.™



# INTRODUCTION

Heat exchanger sooting in 90% multi-poise condensing furnaces can begin to form from several sources. The two most common are improper setup and maintenance, and high sulfur levels in the fuel. The intent of the following information is to address the operational changes of the furnace based on high sulfur levels as well as furnace setup and maintenance. The sources of high sulfur will also be addressed.

## SULFUR LEVEL

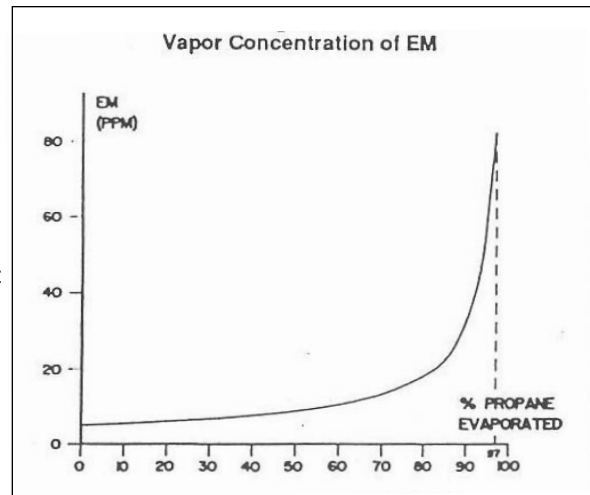
Sulfur is a constituent in fossil fuels, and as long as all processes including refining and distribution are kept in strict control, it will not harm fossil fuel burning equipment. Since Propane has more sulfur transported with it from a variety of sources than Natural Gas, furnaces using Propane for a fuel source may experience sooting more frequently than furnaces using Natural Gas as a fuel source. The highest concentrations of sulfur in Propane come from odorants.

The odorant used in Propane is Ethyl Mercaptan, which is high in sulfur content. Although UL58-78 standard, "Liquid Petroleum Gas Code" suggests that 1 pound of Ethyl Mercaptan should be used per 10,000 gallons of liquid Propane, it is not uncommon for 1.25 to 1.5 pounds or more to be used. Propane distributors want to make sure that if a leak occurs, there is enough odorant to quickly attract the customer's attention. Since there is no regulation of local Propane distribution, this is a common practice.

Ethyl Mercaptan can also accumulate in the storage tank. As this happens, more Ethyl Mercaptan is carried with the Propane to the furnace. National Propane Gas Association information regarding maintenance, cleaning, and recertification of the Propane storage tanks does not address regular purging and cleaning of the interior of the tank so the Propane distributors are left to clean the storage tanks as they deem necessary.

Excess Ethyl Mercaptan can also enter the furnace as the level of Propane in the storage tank is reduced. As figure 3 indicates, when the Propane storage tank is approximately 20% full, the level of Ethyl Mercaptain in the Propane entering the furnace drastically increases.

This study used a clean storage tank and the recommended 1 pound of Ethyl Mercaptan per 10,000 gallons liquid Propane. The increased concentration of sulfur in the Propane increases the dew point temperature of the flue gas. With the increased dew point temperature, the flue gas begins to condense at the inlets of the secondary heat exchanger. The furnace is designed so that the flue gas should begin to condense after it is approximately 1/3 of the way through the secondary heat exchanger.



*Example: Starting with clean tank and recommended 1 lb Ethyl Mercaptan per 10,000 gallons liquid LP gas.  
Odorant Vapor Liquid Equilibria a Generalized Treatment by John Jacobus and David Swienton of Craddock, Heyer and Associates, Kingwood, Texas.*

The flue gas condensate will have sulfur in it. The sulfur in the condensate forms sulfuric acid. Sulfuric acid does not readily evaporate. As the furnace continues to operate, this sulfuric acid solution becomes more concentrated. Levels of sulfuric acid in the condensate samples returned for analysis ranged from 14.3 to 870 Parts per Million. Analysis of one of the returned corroded furnace components found 2700ppm of sulfuric acid.

The concentration of sulfuric acid in the area of the primary cell outlet, cold spot baffle, coupling box, and secondary heat exchanger inlet can cause them to corrode (see example 1). This sulfuric acid attacks unprotected areas of the secondary heat exchanger and can cause the polypropylene to separate from the base metal (see example 2).

When the corrosion from these components begins to block the heat exchanger passages, the amount of air available for proper combustion is reduced. The condensing furnaces are designed to operate with excess air greater than 60%. When the excess air is reduced to below 30%, sooting can start. The corrosion and soot block additional heat exchanger passages until the furnace fails to operate properly.

The pressure switch will not prevent the furnace from operating since this heat exchanger blockage will cause the pressure differential across the heat exchanger to increase.

Visual inspection of the burners will not indicate reduced excess air until they begin to develop yellow tipping or sooting. Combustion analysis is necessary to determine excess air levels.

Refer to Attachment A for information regarding combustion testing and excess air.



**Example 1:** Corrosion on cold spot baffle



**Example 2:** PPL separated from base metal due to sulphuric acid attack

## PROPER SETUP AND MAINTENANCE

When installing the furnace, it is necessary to verify that it is set up properly. The combustion system and the airflow system should be inspected. The use of a gas furnace check list similar to Attachment B at the time of installation is useful to establish a baseline. During routine maintenance or during a service call, this baseline can be used to identify any change in performance. Refer to Attachment C for additional items to check regarding Burner Operation and Proper Excess Air.

Inspection of the drain system, trap, and associated tubing should also be performed. A drain that is plugged or slow to drain allows condensate to build up in the secondary heat exchanger and collector box.

The excess condensate in the heat exchanger or collector box reduces the amount of air moving through the heat exchangers. Visual inspection of the burners will not indicate reduced excess air until they begin to develop yellow tipping or sooting. Combustion analysis is necessary to determine excess air. The condensing furnaces are designed to operate with excess air greater than 60%. When the excess air is reduced to below 30%, sooting can start.

During initial furnace setup and routine maintenance, combustion analysis should be performed. Refer to Attachment A for information regarding combustion testing and excess air.

When converting the furnace to Propane, it is important to follow the current conversion kit instructions. It is important to follow specific instructions for items such as diverter plate, air shutter position, spoiler screws, orifice size, manifold pressure, and installation of the low pressure gas switch along with all instructions for the model and size of furnace that is being converted. The upflow and downflow furnaces must be installed so that they are pitched up to 1/2" toward the front of the furnace to insure proper drainage. Horizontal furnaces must be installed so that they are pitched 1/4" to 1/2" towards the front of the furnace.

<b>Furnace BTUH Input</b>	<b>Approximate Condensate</b>
<b>40,000</b>	<b>3 gal/day</b>
<b>60,000</b>	<b>4.5 gal/day</b>
<b>80,000</b>	<b>6.0 gal/day</b>
<b>100,000</b>	<b>7.5 gal/day</b>
<b>120,000</b>	<b>9 gal/day</b>
<b>140,000</b>	<b>10 gal/day</b>

# ATTACHMENT A

## COMBUSTION ANALYSIS

The furnace must be operating at steady state

- At least 15 min of operation
- Temperature rise at mid-point or slightly above

Perform combustion analysis

- Insert probe of combustion analyzer
- Preferred location is 12" away from inducer outlet
- Exhaust termination can be used for side wall terminations

Excess air should be above 30%

- Refer to the following information for excess air conversion

Excess air below 30% can result in poor burner performance and/or sooting

Propane HD-5 CO2 / EXCESS AIR			
CO2 %	Excess Air %	CO2 %	Excess Air %
11.30	20.0	8.91	50.0
11.20	21.0	8.84	51.0
11.10	22.0	8.78	52.0
11.00	23.0	8.72	53.0
10.91	24.0	8.66	54.0
10.81	25.0	8.60	55.0
10.72	26.0	8.54	56.0
10.63	27.0	8.49	57.0
10.54	28.0	8.43	58.0
10.46	29.0	8.37	59.0
10.37	30.0	8.32	60.0
10.28	31.0	8.26	61.0
10.20	32.0	8.21	62.0
10.12	33.0	8.16	63.0
10.04	34.0	8.10	64.0
9.96	35.0	8.05	65.0
9.88	36.0	8.00	66.0
9.81	37.0	7.95	67.0
9.73	38.0	7.90	68.0
9.65	39.0	7.85	69.0
9.58	40.0	7.80	70.0
9.51	41.0	7.75	71.0
9.44	42.0	7.71	72.0
9.37	43.0	7.66	73.0
9.30	44.0	7.61	74.0
9.23	45.0	7.57	75.0
9.16	46.0	7.52	76.0
9.10	47.0	7.48	77.0
9.03	48.0	7.43	78.0
8.97	49.0	7.39	79.0

Propane HD-5 O2 / EXCESS AIR			
O2 %	Excess Air %	O2 %	Excess Air %
3.76	20.0	7.41	50.0
3.92	21.0	7.51	51.0
4.07	22.0	7.60	52.0
4.21	23.0	7.70	53.0
4.36	24.0	7.79	54.0
4.50	25.0	7.88	55.0
4.64	26.0	7.97	56.0
4.78	27.0	8.05	57.0
4.92	28.0	8.14	58.0
5.05	29.0	8.23	59.0
5.18	30.0	8.31	60.0
5.31	31.0	8.39	61.0
5.44	32.0	8.48	62.0
5.56	33.0	8.56	63.0
5.68	34.0	8.64	64.0
5.81	35.0	8.72	65.0
5.92	36.0	8.79	66.0
6.04	37.0	8.87	67.0
6.16	38.0	8.95	68.0
6.27	39.0	9.02	69.0
6.38	40.0	9.10	70.0
6.49	41.0	9.17	71.0
6.60	42.0	9.24	72.0
6.71	43.0	9.31	73.0
6.81	44.0	9.38	74.0
6.92	45.0	9.45	75.0
7.02	46.0	9.52	76.0
7.12	47.0	9.59	77.0
7.22	48.0	9.66	78.0
7.32	49.0	9.72	79.0

Natural Gas CO2 / Excess Air			
CO2 %	Excess Air %	CO2 %	Excess Air %
9.73	20.0	7.65	50.0
9.65	21.0	7.59	51.0
9.56	22.0	7.54	52.0
9.48	23.0	7.49	53.0
9.39	24.0	7.44	54.0
9.31	25.0	7.38	55.0
9.23	26.0	7.33	56.0
9.15	27.0	7.28	57.0
9.07	28.0	7.23	58.0
9.00	29.0	7.19	59.0
8.92	30.0	7.14	60.0
8.85	31.0	7.09	61.0
8.78	32.0	7.04	62.0
8.71	33.0	7.00	63.0
8.64	34.0	6.95	64.0
8.57	35.0	6.91	65.0
8.50	36.0	6.86	66.0
8.43	37.0	6.82	67.0
8.37	38.0	6.78	68.0
8.30	39.0	6.73	69.0
8.24	40.0	6.69	70.0
8.17	41.0	6.65	71.0
8.11	42.0	6.61	72.0
8.05	43.0	6.57	73.0
7.99	44.0	6.53	74.0
7.93	45.0	6.49	75.0
7.87	46.0	6.45	76.0
7.82	47.0	6.41	77.0
7.76	48.0	6.37	78.0
7.70	49.0	6.34	79.0

Natural Gas O2 / Excess Air			
O2 %	Excess Air %	O2 %	Excess Air %
3.82	20.0	7.50	50.0
3.97	21.0	7.59	51.0
4.12	22.0	7.69	52.0
4.27	23.0	7.78	53.0
4.42	24.0	7.87	54.0
4.56	25.0	7.96	55.0
4.71	26.0	8.05	56.0
4.85	27.0	8.14	57.0
4.98	28.0	8.23	58.0
5.12	29.0	8.31	59.0
5.25	30.0	8.40	60.0
5.38	31.0	8.48	61.0
5.51	32.0	8.56	62.0
5.63	33.0	8.65	63.0
5.76	34.0	8.73	64.0
5.88	35.0	8.81	65.0
6.00	36.0	8.88	66.0
6.12	37.0	8.96	67.0
6.23	38.0	9.04	68.0
6.35	39.0	9.11	69.0
6.46	40.0	9.19	70.0
6.57	41.0	9.26	71.0
6.68	42.0	9.33	72.0
6.79	43.0	9.40	73.0
6.89	44.0	9.47	74.0
7.00	45.0	9.54	75.0
7.10	46.0	9.61	76.0
7.20	47.0	9.68	77.0
7.30	48.0	9.75	78.0
7.40	49.0	9.82	79.0

**ATTACHMENT B  
GAS FURNACE CHECKLIST**

Distributor Name \_\_\_\_\_

Distributor Address \_\_\_\_\_

Dealer Name \_\_\_\_\_

LP Tank Level - % of Full \_\_\_\_\_ Use LP Low Cutoff Switch? Y \_\_\_\_\_ / N \_\_\_\_\_

Customer Name \_\_\_\_\_

Customer Address \_\_\_\_\_

MODEL # \_\_\_\_\_ SERIAL # \_\_\_\_\_ SERIES \_\_\_\_\_

Date of Original Installation \_\_\_\_\_

New Construction *OR* Replacement Furnace

Type of Fuel (circle one) Natural Gas *OR* Propane

Fuel Supplier \_\_\_\_\_

**Furnace Location:**

(circle one for each category)

BASEMENT      ATTIC

UTILITY ROOM      GARAGE

CRAWL SPACE      CLOSET

**Furnace Position:**

UPFLOW      DOWNFLOW

HORIZONTAL      RIGHT      OR      LEFT

**Furnace Vent System - PVC**

VENT TYPE:      DIRECT VENT (2-PIPE)      NON-DIRECT VENT (1-PIPE)

PVC:      Long radius ells?      Y      N      (circle one)

Pipe Dia \_\_\_\_\_      # of Elbows \_\_\_\_\_      Total Length \_\_\_\_\_ ft.

Termination Type: (circle one)      Concentric      *OR*      2-pipe (std)

Termination Location: (circle one)      Roof \_\_\_\_\_      Sidewall\*\* \_\_\_\_\_

\*\*Ht. Above Grade \_\_\_\_\_      # of Combustion Air Disks installed \_\_\_\_\_

**ATTACHMENT B**  
**GAS FURNACE CHECKLIST**

Condensate Trap Location? Left side, Right Side, Blower Shelf, Bottom

Verify condition of Drain Trap, all Rubber Tubing, and Drain Hoses.

Description of surrounding area of termination if sidewall vented:  
shrubs, swimming pool, another appliance vent, etc.

---

---

High Fire \_\_\_\_\_btu/hr Low Fire\_\_\_\_\_btu/hr

MANIFOLD PRESSURE: High Fire\_\_\_\_\_ " W.C. Low Fire\_\_\_\_\_ " W.C.

SUPPLY PRESSURE\*\* \_\_\_\_\_ " W.C. ORIFICE # \_\_\_\_\_

\*\*Supply pressure should be checked with all other gas appliances running clocking gas meter

GAS PIPE SIZE AND LENGTH FROM GAS METER TO APPLIANCE

Dia\_\_\_\_\_ Ft Pipe\_\_\_\_\_

TOTAL (COMBINED) GAS INPUT OF ALL GAS APPLIANCES AT SITE

\_\_\_\_\_BTU

LEAVING AIR TEMPERATURE\_\_\_\_\_ (F) high \_\_\_\_\_ (F) low

RETURN AIR TEMPERATURE\_\_\_\_\_ (F) high \_\_\_\_\_ (F) low

STEADY STATE - AFTER 10 MINUTES OF OPERATION

TEMPERATURE RISE \_\_\_\_\_ (F) high fire

\_\_\_\_\_ (F) low fire

\*\*Temperature rise is equal to the supply air temp minus the return air temp at steady state operation.

The supply temp should be measured away from the line of sight of the Heat Exchanger.

Excess air % _____
--------------------

## ATTACHMENT C

### ADDITIONAL ITEMS TO INSPECT

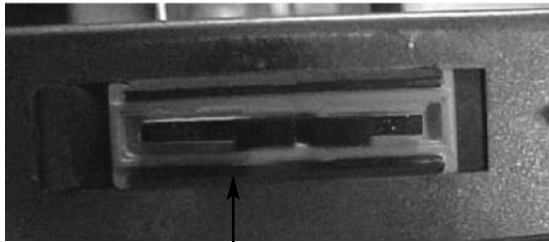
#### BURNER OPERATION:

##### Burners

- Inspect burner flame retainer for corrosion
- Inspect burner flame retainer for blocked splines
- Crossover gap (thickness of a dime)

##### Burner Box Leaks

- Inspect igniter gasket



*Note how gasket seals across the entire base of igniter*

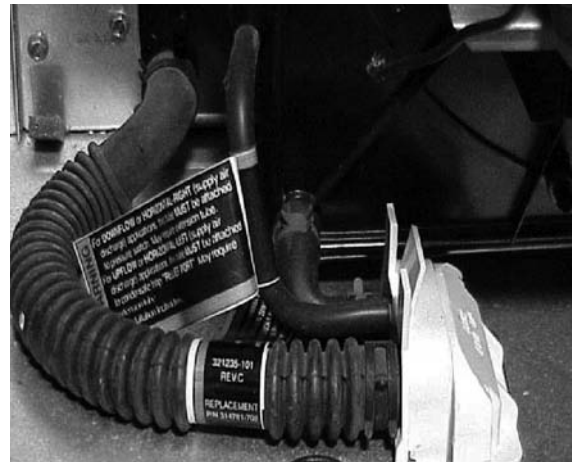
##### New gasket design 2/27/2004

- Inspect seal between burner box and cell panel
- Inspect seal between manifold and burner box
- Insure manifold and orifices are in alignment
- Insure the LP conversion is complete:
  - Correct orifice size
  - Correct manifold pressure
  - Air shutter properly positioned
  - Diverter plate installed
  - Spoiler screws installed
  - Low pressure gas switch installed



## PROPER EXCESS AIR (30% MINIMUM)

- Inspect for proper venting. Verify pipe size based on the tables in the Installation, start-up, and operating instruction manuals.
- Inspect drain
- Slow drains result in lower excess air level
- Debris found in traps of sooted furnaces
- Slow drain allow condensate to fill up secondary heat exchanger
- Verify condition of all tubing
- Verify that drain trap and drain line are clear and primed
- Inspect for leaks at coupling box
- Inspect for restricted secondary heat exchanger inlet or outlet





[www.carrier.com](http://www.carrier.com)

A member of the United Technologies Corporation family.  
Stock Symbol UTX.



© Carrier Corporation 2006

01-858-454-25

Manufacturer reserves the right to discontinue, or change at any time, specifications or designs without notice or without incurring obligations.